

**AMENDMENT TO THE CLAIMS:**

The following claim set replaces all prior versions, and listings, of claims in the application:

1. (Currently Amended) Process for separating  $\text{NH}_3$  from a mixture containing  $\text{NH}_3$ ,  $\text{CO}_2$  and  $\text{H}_2\text{O}$  which comprises an  $\text{NH}_3$  rectification step carried out in an  $\text{NH}_3$  separation device to which one or more streams containing  $\text{NH}_3$ ,  $\text{CO}_2$  and  $\text{H}_2\text{O}$ , including the mixture, are fed from elsewhere in the process, with a stream consisting substantially of gaseous  $\text{NH}_3$  being formed in the  $\text{NH}_3$  separation device, separated from the mixture and discharged, characterized in that a condensation step is carried out on at least one of the stream consisting substantially of gaseous  $\text{NH}_3$  or the one or more streams containing  $\text{NH}_3$ ,  $\text{CO}_2$  and  $\text{H}_2\text{O}$  supplied to the  $\text{NH}_3$  separation device, in which at least a part of the existing  $\text{CO}_2$  is converted to a liquid phase.

2. (original) Process according to claim 1, in which the condensation step is carried out by cooling the stream to be condensed and/or bringing it into contact with an absorbing medium.

3. (previously presented) Process according to claim 1, the process further comprising, in order to separate  $\text{CO}_2$  and  $\text{H}_2\text{O}$  from the mixture:

a  $\text{CO}_2$  rectification step, which is applied in a  $\text{CO}_2$  separation device to the mixture coming from the  $\text{NH}_3$  separation device while a stream coming from a desorption device is supplied, with a stream consisting substantially of  $\text{CO}_2$  being formed in the  $\text{CO}_2$  separation device and being separated from the mixture, and

a desorption step, which is applied in the desorption device to the mixture coming from the  $\text{CO}_2$  separation device, with a stream consisting substantially of  $\text{H}_2\text{O}$  being formed and being separated from the mixture, after which the mixture is returned to the  $\text{NH}_3$  separation device and/or the  $\text{CO}_2$  separation device,

in which the condensation step is carried out on the stream consisting substantially of gaseous  $\text{NH}_3$  from the  $\text{NH}_3$  separation device and/or on at least a part of the stream that comes from the desorption device and that is supplied to the  $\text{NH}_3$  separation device.

4. (previously presented) Process according to claim 1, in which the condensation step is carried out on the stream consisting substantially of gaseous  $\text{NH}_3$  from the  $\text{NH}_3$  separation device in a submerged condenser while an aqueous stream and/or liquid  $\text{NH}_3$  is supplied as absorbing medium.

5. (original) Process according to claim 4, in which after the condensation step an absorption step is applied to the stream consisting substantially of gaseous  $\text{NH}_3$ , in which the said stream is brought into contact with liquid  $\text{NH}_3$ .

6. (currently amended) Process according to claim 1, in which the condensation step is carried out as a partial condensation step, by means of indirect cooling with a cooling medium, on ~~the~~ a stream that comes from ~~the~~ a desorption device and ~~that~~ is supplied to the  $\text{NH}_3$  separation device.

7. (original) Process according to claim 6, in which the mixture present in the  $\text{NH}_3$  separation device is used as cooling medium in the partial condensation step.